CPC COOPERATIVE PATENT CLASSIFICATION

F MECHANICAL ENGINEERING; LIGHTING; HEATING; WEAPONS; BLASTING (NOTE omitted)

LIGHTING; **HEATING**

- F25 REFRIGERATION OR COOLING; COMBINED HEATING AND REFRIGERATION SYSTEMS; HEAT PUMP SYSTEMS; MANUFACTURE OR STORAGE OF ICE; LIQUEFACTION SOLIDIFICATION OF GASES
- F25J LIQUEFACTION, SOLIDIFICATION OR SEPARATION OF GASES OR GASEOUS {OR LIQUEFIED GASEOUS} MIXTURES BY PRESSURE AND COLD TREATMENT {OR BY BRINGING THEM INTO THE SUPERCRITICAL STATE (cryogenic pumps F04B 37/08; gas storage vessels, gas holders F17; filing vessels with, or discharging from vessels, compressed, liquefied or solidified gases F17C; refrigeration machines, plants, or systems F25B)}

WARNING

In this subclass non-limiting references (in the sense of paragraph 39 of the Guide to the IPC) may still be displayed in the scheme.

1/00	Processes or apparatus for liquefying or solidifying	1/0057	• • • { after expansion of the liquid refrigerant
	gases or gaseous mixtures {(recovering volatile		stream with extraction of work}
	solvents by condensation <u>B01D 5/00</u> ; vapor recovery	1/006	• {characterised by the refrigerant fluid used
	systems combined with filling nozzles <u>B67D 7/54</u> ;		(refrigerants in vapor compression cycles
	solidification of carbonic acid <u>C01B 32/55</u> ; for		<u>F25B 9/002</u> , refrigerant materials <u>per se</u>
	ammonia in general <u>C01C 1/00</u>)}		<u>C09K 5/00</u>)}
1/0002	 {characterised by the fluid to be liquefied} 	1/0062	 {Light or noble gases, mixtures thereof
1/0005	• • {Light or noble gases (F25J 1/0012 takes		$(\underline{F25J \ 1/007} \ takes \ precedence)$
	precedence)}	1/0065	{Helium}
1/0007	{Helium}	1/0067	{Hydrogen}
1/001	{Hydrogen}	1/007	• • {Primary atmospheric gases, mixtures thereof}
1/0012	• • {Primary atmospheric gases, e.g. air}	1/0072	{Nitrogen}
1/0015	{Nitrogen}	1/0075	{Oxygen}
1/0017	{Oxygen}	1/0077	{Argon}
1/002	{Argon}	1/008	• • {Hydrocarbons}
1/0022	• {Hydrocarbons, e.g. natural gas}	1/0082	{Methane}
1/0025	{Boil-off gases "BOG" from storages}	1/0085	{Ethane; Ethylene}
1/0023	• • {Oxides of carbon, e.g. CO ₂ }	1/0087	{Propane; Propylene}
1/0027	• {Characterised by the kind of cold generation within	1/0087	{Hydrocarbons with four or more carbon
1/003	the liquefaction unit for compensating heat leaks	1/009	atoms}
	and liquid production}	1/0092	• • {Mixtures of hydrocarbons comprising possibly
1/0032	 • {using the feed stream itself or separated fractions 	1/0092	also minor amounts of nitrogen
1/0032	from it, i.e. "internal refrigeration"}	1/0095	• • {Oxides of carbon, e.g. CO ₂ }
1/0035	• • {by gas expansion with extraction of work}	1/0093	
1/0033	{of a return stream}	1/0097	• • {Others, e.g. F-, Cl-, HF-, HClF-, HCl- hydrocarbons etc. or mixtures thereof}
		1/02	
1/004	• • • {by flash gas recovery (<u>F25J 1/0267</u> takes precedence)}	1/02	 requiring the use of refrigeration, e.g. of helium or hydrogen {; Details and kind of the refrigeration
1/0042	•		system used; Integration with other units or
	• • {by liquid expansion with extraction of work}		processes; Controlling aspects of the process}
1/0045	• • {by vaporising a liquid return stream}	1/0201	• • {using only internal refrigeration means, i.e.
1/0047	{using an "external" refrigerant stream in a	1/0201	without external refrigeration means, i.e.
	closed vapor compression cycle (<u>F25J 1/0221</u> ,	1/0202	{in a quasi-closed internal refrigeration loop
1/005	F25J 1/0225 take precedence)}	1/0202	(F25J 1/0208, F25J 1/0219, F25J 1/0224 take
1/005	• • • {by expansion of a gaseous refrigerant stream		(<u>P253 1/0208</u> , <u>P253 1/0219</u> , <u>P253 1/0224</u> take precedence)}
1/0053	with extraction of work}		procedence);
1/0052	• • • {by vaporising a liquid refrigerant stream}		

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 $1/0055 \qquad \hbox{. . . .} \ \{ originating \ from \ an \ incorporated \ cascade \}$

1/0203	• • {using a single-component refrigerant [SCR] fluid in a closed vapor compression cycle (F25J 1/0211 takes precedence)}	1/0237	{integrating refrigeration provided for liquefaction and purification/treatment of the gas to be liquefied, e.g. heavy hydrocarbon
1/0204			removal from natural gas (details related
1/0204	• • • {as a single flow SCR cycle}		to rectification F25J 3/02; details related to
1/0205	• • • {as a dual level SCR refrigeration cascade}		
1/0207	• • • {as at least a three level SCR refrigeration cascade}		partial condensation <u>F25J 3/06</u> ; working-up natural gas <u>C10L 3/10</u>)}
1/0208	 . • {in combination with an internal quasi-closed refrigeration loop, e.g. with deep flash recycle loop (F25J 1/021 takes precedence)} . • {as at least a three level refrigeration 	1/0238	• • • • • {Purification or treatment step is integrated within one refrigeration cycle only, i.e. the same or single refrigeration cycle provides feed gas cooling (if present)
	cascade}	1/0239	and overhead gas cooling} {Purification or treatment step being}
1/021	• • • • {using a deep flash recycle loop}	1/0237	integrated between two refrigeration
1/0211	• { using a multi-component refrigerant [MCR] fluid in a closed vapor compression cycle}		cycles of a refrigeration cascade, i.e. first cycle providing feed gas cooling and
1/0212	• • • {as a single flow MCR cycle}		second cycle providing overhead gas
1/0214	• • • {as a dual level refrigeration cascade with at		cooling}
	least one MCR cycle}	1/0241	{wherein the overhead cooling
1/0215	• • • { with one SCR cycle }	-,	comprises providing reflux for a
1/0216	• • • • {using a C3 pre-cooling cycle}		fractionation step}
1/0217	• • • { as at least a three level refrigeration cascade	1/0242	
	with at least one MCR cycle}	1/0242	{Waste heat recovery, e.g. from heat of compression}
1/0218	• • • { with one or more SCR cycles, e.g. with a	1/0243	• • {Start-up or control of the process; Details of
	C3 pre-cooling cycle}		the apparatus used; Details of the refrigerant
1/0219	• • • {in combination with an internal quasi-closed		compression system used}
	refrigeration loop, e.g. using a deep flash	1/0244	{Operation; Control and regulation;
	recycle loop}	1,02	Instrumentation (F25J 1/0279 takes
1/0221	• • {using the cold stored in an external cryogenic		precedence)}
	component in an open refrigeration loop}	1/0245	{Different modes, i.e. 'runs', of operation;
1/0222	• • • {in combination with an intermediate heat	1/0243	Process control}
	exchange fluid between the cryogenic	1/0247	•
	component and the fluid to be liquefied		• • • • {start-up of the process}
	(F25J 1/0224 takes precedence)	1/0248	{Stopping of the process, e.g. defrosting or deriming, maintenance; Back-up mode or
1/0223	{in combination with the subsequent re-		systems}
	vaporisation of the originally liquefied gas	1/0249	• • • • • • • Controlling refrigerant inventory, i.e.
	at a second location to produce the external	1/0249	composition or quantity (charging or
	cryogenic component}		discharging refrigerants in cooling systems
1/0224	• • • {in combination with an internal quasi-closed		
1,022.	refrigeration loop (F25J 1/0208, F25J 1/0219	1 100 -	<u>F25B 45/00</u>)}
		1/025	{Details related to the refrigerant
1 /0225	take precedence)}		production or treatment, e.g. make-up
1/0225	• • {using other external refrigeration means not		supply from feed gas itself}
	provided before, e.g. heat driven absorption	1/0251	{Intermittent or alternating process, so-
	chillers}		called batch process, e.g. "peak-shaving"}
1/0227	• • { within a refrigeration cascade }	1/0252	{Control strategy, e.g. advanced process
1/0228	• • {Coupling of the liquefaction unit to other units	1,0202	control or dynamic modeling}
	or processes, so-called integrated processes	1/0254	• • • {controlling particular process parameter,
	(combined plants, e.g. engine plant combined	1/0254	e.g. pressure, temperature}
	with an industrial process <u>F01K 23/064</u> ;	1/0255	• • • • {controlling the composition of the feed or
	gas turbine plants in combination with other	1/0233	liquefied gas, e.g. to achieve a particular
	processes <u>F02C 6/00</u>)}		
1/0229	• • • {Integration with a unit for using hydrocarbons,	1 /02 5 6	heating value of natural gas}
	e.g. consuming hydrocarbons as feed stock}	1/0256	• • • {Safety aspects of operation (F25J 1/0298
1/023	• • • • {for the combustion as fuels, i.e. integration		takes precedence)}
1/023	with the fuel gas system}	1/0257	• • • {Construction and layout of liquefaction
1/0221			equipments, e.g. valves, machines (F25J 1/0279
1/0231	• • • { for the working-up of the hydrocarbon feed,		takes precedence)}
	e.g. reinjection of heavier hydrocarbons into	1/0258	• • • {vertical layout of the equipments within in
	the liquefied gas}		the cold box}
1/0232	• • • {integration within a pressure letdown station	1/0259	{Modularity and arrangement of parts of
	of a high pressure pipeline system}	1,0237	the liquefaction unit and in particular of the
1/0234	{Integration with a cryogenic air separation		cold box, e.g. pre-fabrication, assembling
	unit (cryogenic separation of air <u>F25J 3/04</u>)}		and erection, dimensions, horizontal layout
1/0235	{Heat exchange integration}		
1/0236	• • • {providing refrigeration for different		"plot"}
1,0230	processes treating not the same feed stream}		

processes treating not the same feed stream}

1/0261	• • • {Details of cold box insulation, housing and internal structure (buildings forming parts of	1/0291	• • • {Refrigerant compression by combined gas compression and liquid pumping}
	cooling plants E04H 5/10)}	1/0292	{Refrigerant compression by cold or
1/0262	• • • • {Details of the cold heat exchange system (constructional details <u>F25J 5/00</u> ,	1/0294	cryogenic suction of the refrigerant gas} {Multiple compressor casings/strings in
	construction of cold-exchangers in general		parallel, e.g. split arrangement}
1/0263	F28)} {using different types of heat exchangers}	1/0295	• • • • {Shifting of the compression load between different cooling stages within a refrigerant
1/0264	• • • • { Arrangement of heat exchanger cores in parallel with different functions, e.g.		cycle or within a cascade refrigeration system}
	different cooling streams (F25J 1/0272	1/0296	• • • • {Removal of the heat of compression, e.g.
1/0265	takes precedence)} {comprising cores associated		within an inter- or afterstage-cooler against an ambient heat sink}
	exclusively with the cooling of a refrigerant stream, e.g. for auto-	1/0297	• • • • {using an externally chilled fluid, e.g.
	refrigeration or economizer}	1/0298	chilled water} {Safety aspects and control of the refrigerant
1/0267 1/0268	{using flash gas as heat sink} {using a dedicated refrigeration		compression system, e.g. anti-surge control}
1/0208	means (<u>F25J 1/0296</u> takes precedence)}	3/00	Processes or apparatus for separating the constituents of gaseous {or liquefied gaseous} mixtures involving the use of liquefaction or
1/0269	• • • {Arrangement of liquefaction units or equipments fulfilling the same process step,		solidification
	e.g. multiple "trains" concept (F25J 1/0294	3/02	 by rectification, i.e. by continuous interchange of heat and material between a vapour stream and
1/027	takes precedence)} {Inter-connecting multiple hot equipments		a liquid stream (<u>F25J 3/08</u> takes precedence {;
1 (0.2.7.1	upstream of the cold box}	3/0204	 purification of hydrocarbons in general <u>CO7C 7/00</u>}) . {characterised by the feed stream (for air
1/0271	• • • • • {Inter-connecting multiple cold equipments within or downstream of the		<u>F25J 3/04</u>)}
1./0252	cold box}	3/0209 3/0214	 {Natural gas or substitute natural gas} {Liquefied natural gas}
1/0272	{Multiple identical heat exchangers in parallel}	3/0219	• • • {Refinery gas, cracking gas, coke oven
1/0274	• • • • {Retrofitting or revamping of an existing liquefaction unit}		gas, gaseous mixtures containing aliphatic unsaturated CnHm or gaseous mixtures of undefined nature}
1/0275	• • • {adapted for special use of the liquefaction unit, e.g. portable or transportable devices}	3/0223	• • • {H ₂ /CO mixtures, i.e. synthesis gas; Water
1/0276	• • • • {Laboratory or other miniature devices}		gas or shifted synthesis gas (production of carbon monoxide containing gas in general
1/0277 1/0278	 {Offshore use, e.g. during shipping} {Unit being stationary, e.g. on floating		<u>C01B 32/40</u> , <u>C10J</u> , <u>C10K</u> ; production of
	barge or fixed platform}	3/0228	hydrogen containing gas <u>C01B 3/00</u>)} {characterised by the separated product stream}
1/0279	 {Compression of refrigerant or internal recycle fluid, e.g. kind of compressor, accumulator, suction drum etc.} 	3/0233	{separation of CnHm with 1 carbon atom or more}
1/0281	• • • {characterised by the type of prime driver,	3/0238	 . • {separation of CnHm with 2 carbon atoms or more}
1/0282	e.g. hot gas expander} {Steam turbine as the prime mechanical	3/0242	• • { separation of CnHm with 3 carbon atoms or
	driver}	3/0247	more } {separation of CnHm with 4 carbon atoms or
1/0283	{Gas turbine as the prime mechanical driver}		more}
1/0284	• • • • {Electrical motor as the prime mechanical driver}	3/0252	 . • (separation of hydrogen (production of hydrogen containing gas in general <u>C01B 3/00</u>, e.g. separation of hydrogen or hydrogen
1/0285	• • • • {Combination of different types of drivers mechanically coupled to the same refrigerant		containing gases form gaseous mixtures at low
	compressor, possibly split on multiple	3/0257	temperatures <u>C01B 3/506</u>)} {separation of nitrogen (from air <u>F25J 3/04</u> ,
1/0287	compressor casings} {including an electrical motor}		production of nitrogen in general <u>C01B 21/00</u>)}
1/0288	• • • • {using work extraction by mechanical	3/0261	• • • {separation of carbon monoxide (production of carbon monoxide containing gas in general
	coupling of compression and expansion of the refrigerant, so-called companders}		<u>C01B 32/40, C10J, C10K</u>)}
1/0289	• • • {Use of different types of prime drivers of	3/0266	• • • {separation of carbon dioxide (production of carbon dioxide in general <u>C01B 32/00</u>)}
	at least two refrigerant compressors in a cascade refrigeration system}	3/0271	• • • {separation of H ₂ /CO mixtures, i.e. of synthesis
1/029	(Mechanically coupling of different		gas (production of carbon monoxide containing gas in general C01B 32/40, C10J, C10K,
	refrigerant compressors in a cascade refrigeration system to a common driver}		production of hydrogen containing gas
			<u>C01B 3/00</u>)}

3/0276 {separation of H_2/N_2 mixtures, i.e. of ammonia	3/04157 { Afterstage cooling and so-called "pre-
synthesis gas (in general <u>C01B 3/00</u>)} 3/028 {separation of noble gases (from air	cooling" of the feed air upstream the air purification unit and main heat exchange line
F25J 3/04642; in general C01B 23/00)}	(<u>F25J 3/04618</u> takes precedence)}
3/0285 {of argon}	3/04163 {Hot end purification of the feed air
3/029 {of helium}	(arrangements of cold regenerators
3/0295 • • {Start-up or control of the process; Details of the	F25J 5/00)} 3/04169 {by adsorption of the impurities
apparatus used, e.g. sieve plates, packings} 3/04 • for air	(adsorption in general <u>B01D 53/02</u>)}
3/04006 {Providing pressurised feed air or process	3/04175 {at a pressure of substantially more than
streams within or from the air fractionation	the highest pressure column}
unit}	3/04181 {Regenerating the adsorbents}
3/04012 {by compression of warm gaseous streams;	3/04187 {Cooling of the purified feed air by
details of intake or interstage cooling (F25J 3/04048 takes precedence; operation of	recuperative heat-exchange; Heat-exchange with product streams (arrangements of cold
compressors F25J 3/04781; particular layout	exchangers <u>F25J 5/002</u>)}
of compressors used in air fractionation units	3/04193 {Division of the main heat exchange line
<u>F25J 3/04866</u>)}	in consecutive sections having different
3/04018 {of main feed air}	functions}
3/04024 {of purified feed air, so-called boosted air}	3/042 {having an intermediate feed connection}
3/0403 {of nitrogen}	3/04206 {including a so-called "auxiliary
3/04036 {of oxygen} 3/04042 {of argon or argon enriched stream}	vaporiser" for vaporising and producing
3/04048 {by compression of cold gaseous streams,	a gaseous product}
e.g. intermediate or oxygen enriched (waste)	3/04212 {and simultaneously condensing
streams}	vapor from a column serving as reflux within the or another column}
3/04054 {of air}	3/04218 {Parallel arrangement of the main heat
3/0406 {of nitrogen}	exchange line in cores having different
3/04066 {of oxygen} 3/04072 {of argon or argon enriched stream}	functions, e.g. in low pressure and high
3/04078 {or argon or argon enriched stream}	pressure cores (<u>F25J 3/04503</u> takes
compression and vaporisation with cold	precedence)} 3/04224 {Cores associated with a liquefaction or
recovery, i.e. so-called internal compression	3/04224 {Cores associated with a liquefaction or refrigeration cycle}
(operation of pumps <u>F25J 3/04781</u> ; particular	3/0423 {Subcooling of liquid process streams}
layout of pumps used in air fractionation units F25J 3/04866)}	3/04236 {Integration of different exchangers in
3/04084 {of nitrogen}	a single core, so-called integrated cores
3/0409 {of oxygen}	(F25J 3/04624 takes precedence)} 3/04242 {Cold end purification of the feed air}
3/04096 {of argon or argon enriched stream}	3/04248 {Cold end pulmication of the feed air}
3/04103 • • • • {using solely hydrostatic liquid head}	leaks or liquid production, e.g. by Joule-
3/04109 {Arrangements of compressors and /or their	Thompson expansion}
drivers (using work extraction by mechanical coupling of compression and cold expansion	3/04254 {using the cold stored in external cryogenic
F25J 3/04381)}	fluids (closed loop <u>F25J 3/04278</u>)}
3/04115 {characterised by the type of prime driver,	3/0426 {The cryogenic component does not participate in the fractionation}
e.g. hot gas expander}	3/04266 {and being liquefied hydrocarbons}
3/04121 {Steam turbine as the prime mechanical	3/04272 {and comprising means for reducing
driver} 3/04127 {Gas turbine as the prime mechanical	the risk of pollution of hydrocarbons
driver}	into the air fractionation}
3/04133 {Electrical motor as the prime	3/04278 {using external refrigeration units,
mechanical driver}	e.g. closed mechanical or regenerative refrigeration units}
3/04139 (Combination of different types of	3/04284 {using internal refrigeration by open-loop
drivers mechanically coupled to the same	gas work expansion, e.g. of intermediate
compressor, possibly split on multiple compressor casings}	or oxygen enriched (waste-)streams
3/04145 {Mechanically coupling of different	(F25J 3/04333 takes precedence)}
compressors of the air fractionation	3/0429 { of feed air, e.g. used as waste or product air or expanded into an auxiliary column}
process to the same driver(s)}	3/04296 {Claude expansion, i.e. expanded into
3/04151 {Purification and (pre-)cooling of the feed	the main or high pressure column)
air; recuperative heat-exchange with product streams}	3/04303 {Lachmann expansion, i.e. expanded
ouvering)	into oxygen producing or low pressure
	column} 3/04309 {of nitrogen}
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	{Lowest pressure or impure nitrogen, so-called waste nitrogen expansion}	3/04478 {for controlling purposes, e.g. start-up or back-up procedures (F25J 3/04496 takes
3/04321	• • • • {of oxygen}	precedence)}
3/04327	• • • • { of argon or argon enriched stream}	3/04484 (for purity control during steady state
3/04333	{using quasi-closed loop internal vapor	operation}
	compression refrigeration cycles, e.g. of intermediate or oxygen enriched	3/0449 {for rapid load change of the air fractionation unit}
	(waste-)streams}	3/04496 { for compensating variable air feed or
3/04339		variable product demand by alternating
	{and comprising a gas work expansion	between periods of liquid storage and liquid
5, 0.15.15	loop}	assist}
3/04351	· · · · {of nitrogen}	3/04503 {by exchanging "cold" between at
	{and comprising a gas work expansion	least two different cryogenic liquids,
3/04337	loop}	e.g. independently from the main heat
3/04363	•	exchange line of the air fractionation and/
3/04369		or by using external alternating storage
3/04305		systems}
3/04373	process parameter etc.}	3/04509 {within the cold part of the air
3/04381		fractionation, i.e. exchanging "cold"
3/04381	{using work extraction by mechanical coupling of compression and expansion	within the fractionation and/or main heat
	so-called companders}	exchange line}
2/0/297	• • •	3/04515 (Simultaneously changing air feed
3/04387	expansion}	and products output}
3/04393	* *	3/04521 {Coupling of the air fractionation unit
3/04393	expansion}	to an air gas-consuming unit, so-called
3/044		integrated processes (combined plants, e.g.
3/044	• • • {using a single pressure main column system only (F25J 3/0446, F25J 3/04624,	engine plant combined with an industrial
	F25J 3/04636 take precedence)}	process <u>F01K 23/064</u> ; gas-turbine plants
3/04406		supplying working fluid to a chemical process
3/04400	(F25J 3/0446, F25J 3/04624, F25J 3/04636 and	<u>F02C 6/10</u>)}
	F25J 3/04715 take precedence)}	3/04527 {Integration with an oxygen consuming
3/04412		unit, e.g. glass facility, waste incineration or
3/04412	with thermal coupling by a main reboiler-	oxygen based processes in general}
	condenser in the bottom of low pressure	3/04533 {for the direct combustion of fuels
	respectively top of high pressure column}	in a power plant, so-called "oxyfuel
3/04418		combustion"}
3/04410	pressure columns}	$3/04539$ {for the H ₂ /CO synthesis by partial
3/04424	*	oxidation or oxygen consuming reforming
5/01121	pressure columns, i.e. a so-called split	processes of fuels}
	columns}	3/04545 {for the gasification of solid or heavy
3/0443	{A main column system not otherwise	liquid fuels, e.g. integrated gasification
-, -, -, -,	provided, e.g. a modified double column	combined cycle [IGCC]}
	flowsheet}	3/04551 {for the metal production}
3/04436	• • • {using at least a triple pressure main	3/04557 {for pig iron or steel making, e.g. blast
	column system (<u>F25J 3/0446</u> , <u>F25J 3/04624</u> ,	furnace, Corex}
	F25J 3/04636 and F25J 3/04715 take	3/04563 {Integration with a nitrogen consuming unit,
	precedence)}	e.g. for purging, inerting, cooling or heating}
3/04442	{in a double column flowsheet with a high	3/04569 {for enhanced or tertiary oil recovery}
	pressure pre-rectifier}	3/04575 {for a gas expansion plant, e.g. dilution of
3/04448		the combustion gas in a gas turbine}
	intermediate pressure column}	3/04581 {Hot gas expansion of indirect heated
3/04454		nitrogen}
	provided, e.g. serially coupling of columns or	3/04587 {for the NH ₃ synthesis, e.g. for adjusting
	more than three pressure levels}	the H_2/N_2 ratio}
3/0446	• • • {using the heat generated by mixing two	3/04593 {The air gas consuming unit is also fed by an
	different phases}	air stream}
3/04466		3/046 {Completely integrated air feed
	overhead gas by mixing gaseous air feed and	compression, i.e. common MAC}
	liquid oxygen}	3/04606 {Partially integrated air feed compression,
3/04472	• • • {using the cold from cryogenic liquids	i.e. independent MAC for the air
	produced within the air fractionation unit and	fractionation unit plus additional air feed
	stored in internal or intermediate storages}	from the air gas consuming unit}
		3/04612 {Heat exchange integration with process
		streams, e.g. from the air gas consuming
		unit}

3/04618	• • • • { for cooling an air stream fed to the air fractionation unit }	3/04781 {Pressure changing devices, e.g. for compression, expansion, liquid pumping}
3/04624	• • • {using integrated mass and heat exchange, so-called non-adiabatic rectification, e.g.	3/04787 {Heat exchange, e.g. main heat exchange line; Subcooler, external reboiler-
	dephlegmator, reflux exchanger}	condenser (<u>F25J 3/04793</u> and <u>F25J 3/0486</u>
3/0463	• • • • {Simultaneously between rectifying and stripping sections, i.e. double dephlegmator}	take precedence)} 3/04793 {Rectification, e.g. columns; Reboiler-
3/04636	• • • {using a hybrid air separation unit, e.g. combined process by cryogenic separation	condenser (<u>F25J 3/0486</u> takes precedence)}
	and non-cryogenic separation techniques	3/048 {Argon recovery}
	(F25J 3/04733 and F25J 3/04757 take	3/04806 {High purity argon purification}
	precedence)}	3/04812 {Different modes, i.e. "runs" of operation
3/04642	• • • {Recovering noble gases from air (from	(F25J3/04472 takes precedence)
	gas mixtures other than air F25J 3/028 or	3/04818 {Start-up of the process}
	<u>F25J 3/0685</u>)}	3/04824 {Stopping of the process, e.g. defrosting
3/04648	{argon}	or deriming; Back-up procedures}
3/04654	• • • • {Producing crude argon in a crude argon column}	3/0483 {Rapid load change of the air fractionation unit}
3/0466	• • • • { as a parallel working rectification	3/04836 {Variable air feed, i.e. "load" or product
	column or auxiliary column system in a	demand during specified periods, e.g.
2/04	single pressure main column system}	during periods with high respectively
3/04666	{ as a parallel working rectification column of the low pressure column in a	low power costs (<u>F25J 3/0483</u> takes
	dual pressure main column system}	precedence)}
3/04672	• • • • • • {having a top condenser}	3/04842 {Intermittent process, so-called batch process}
3/04678		3/04848 {Control strategy, e.g. advanced process
5/010/0	liquid from high pressure column	control or dynamic modeling}
	bottoms}	3/04854 {Safety aspects of operation}
3/04684	• • • • • • { and a bottom re-boiler	3/0486 {of vaporisers for oxygen enriched
	$(\underline{F25J \ 3/04696} \ takes \ precedence)$	liquids, e.g. purging of liquids}
3/0469	{ and an intermediate re-boiler/	3/04866 {Construction and layout of air fractionation
	condenser (F25J 3/04696 takes	equipments, e.g. valves, machines (<u>F25J 5/00</u>
3/04696	precedence)} {a bottom re-boiler and an	takes precedence)}
3/04090	intermediate re-boiler/condenser}	3/04872 {Vertical layout of cold equipments within in the cold box, e.g. columns, heat
3/04703	• • • • • • • • {being arranged in more than one	exchangers etc.}
	vessel}	3/04878 {Side by side arrangement of multiple
3/04709	• • • • { as an auxiliary column system in	vessels in a main column system,
	at least a dual pressure main column	wherein the vessels are normally
2/04515	system}	mounted one upon the other or forming
3/04715	{The auxiliary column system simultaneously produces oxygen}	different sections of the same column (multiple vessels of a crude argon
3/04721	• • • • • {Producing pure argon, e.g. recovered	column F25J 3/04703)}
3/01/21	from a crude argon column}	3/04884 {Arrangement of reboiler-condensers}
3/04727		3/0489 {Modularity and arrangement of parts
	for nitrogen rejection (F25J 3/04739)	of the air fractionation unit, in particular
	takes precedence)}	of the cold box, e.g. pre-fabrication,
3/04733	• • • • • {using a hybrid system, e.g. using	assembling and erection, dimensions,
	adsorption, permeation or catalytic reaction}	horizontal layout "plot" (<u>F25J 3/04872</u> takes precedence)}
3/04739		3/04896 {Details of columns, e.g. internals, inlet/
3/04/37	pure argon column}	outlet devices}
3/04745		3/04903 {Plates or trays}
3/04751	• • • • {Producing pure krypton and/or xenon	3/04909 {Structured packings}
	recovered from a crude krypton/xenon	3/04915 (Combinations of different material
	mixture}	exchange elements, e.g. within different
3/04757	• • • • • { using a hybrid system, e.g. using	columns}
	adsorption, permeation or catalytic reaction}	3/04921 { within the same column} 3/04927 {Liquid or gas distribution devices}
3/04763		3/04927 {Liquid or gas distribution devices} 3/04933 {Partitioning walls or sheets}
5/07/03	the apparatus used}	3/04939 {Partitioning wans or sneets}
3/04769	{Operation, control and regulation of the	columns (details of dephlegmators
	process; Instrumentation within the process}	F25J 5/007)}
3/04775	• • • • {Air purification and pre-cooling}	

3/04945	• • • • {Details of internal structure; insulation and housing of the cold box}	3/068	• • • {separation of H ₂ /N ₂ mixtures, i.e. of ammonia synthesis gas (in general C01B 3/00)}
3/04951	• • • • { Arrangements of multiple air fractionation units or multiple equipments	3/0685	• • • {separation of noble gases (from air F25J 3/04642; in general C01B 23/00)}
	fulfilling the same process step, e.g.	3/069	• • • { of helium }
	multiple trains in a network (<u>F25J 3/04636</u> takes precedence)}	3/0695	• • {Start-up or control of the process; Details of the
3/04957	• • • • • {and inter-connecting equipments	3/08	apparatus used} Separating gaseous impurities from gases or
5,0.55,	upstream of the fractionation unit (s), i.e. at the "front-end"}	3/08	gaseous mixtures {or from liquefied gases or liquefied gaseous mixtures}(cold traps <u>B01D 8/00</u>)
3/04963	• • • • {and inter-connecting equipment	5 /00	
	within or downstream of the fractionation unit(s) (F25J 3/04393 takes precedence)}	5/00	Arrangements of cold exchangers or cold accumulators in separation or liquefaction plants (heat exchangers F28C, F28D, F28F)
3/04969	• • • • {Retrofitting or revamping of an existing air fractionation unit}	5/002	• {for continuously recuperating cold, i.e. in a so- called recuperative heat exchanger}
3/04975	• • • • {adapted for special use of the air	5/005	• • {in a reboiler-condenser, e.g. within a column}
3/04973	fractionation unit, e.g. transportable devices by truck or small scale use}	5/007	{combined with mass exchange, i.e. in a so-called dephlegmator}
3/04981	• • • • • {for portable medical or home use}		
3/04987	• • • • • {for offshore use}	2200/00	Processes or apparatus using separation by rectification
3/04993	• • • • • {for space applications, e.g. for rocket	2200/02	in a single pressure main column system
	use}	2200/02	in a dual pressure main column system
3/06	• by partial condensation (F25J 3/08 takes	2200/04	• in a classical double column flow-sheet, i.e. with
	precedence; by rectification <u>F25J 3/02</u> {;	2200/00	thermal coupling by a main reboiler-condenser
3/0605	 purification of hydrocarbons in general <u>C07C 7/00</u>}) . {characterised by the feed stream (for air 		in the bottom of low pressure respectively top of
3/0003	F25J 3/04)}		high pressure column
3/061	• • {Natural gas or substitute natural gas}	2200/08	in a triple pressure main column system
3/0615	{Liquefied natural gas}	2200/10	• in a quadruple, or more, column or pressure system
3/062	{Refinery gas, cracking gas, coke oven	2200/20	in an elevated pressure multiple column system
	gas, gaseous mixtures containing aliphatic		wherein the lowest pressure column is at a pressure well above the minimum pressure needed to
	unsaturated CnHm or gaseous mixtures of		overcome pressure drop to reject the products to
2/0/25	undefined nature}		atmosphere
3/0625	• • • {H ₂ /CO mixtures, i.e. synthesis gas; Water	2200/30	using a side column in a single pressure column
	gas or shifted synthesis gas (production of carbon monoxide containing gas in general		system
	C01B 32/40, C10J, C10K; production of hydrogen containing gas C01B 3/00)}	2200/32	• using a side column fed by a stream from the high pressure column
3/063	• • {characterised by the separated product stream}	2200/34	• using a side column fed by a stream from the low
3/0635	• • { separation of CnHm with 1 carbon atom or		pressure column
	more}	2200/38	using pre-separation or distributed distillation before
3/064	• • • {separation of CnHm with 2 carbon atoms or more}		a main column system, e.g. in a at least a double column system
3/0645	• • • { separation of CnHm with 3 carbon atoms or	2200/40	Features relating to the provision of boil-up in the bottom of a column
2/065	more)	2200/50	. using multiple (re-)boiler-condensers at different
3/065	{separation of CnHm with 4 carbon atoms or more}		heights of the column
3/0655	• • • {separation of hydrogen (production of	2200/52	in the high pressure column of a double pressure
	hydrogen containing gas in general C01B 3/00,	2200/54	main column system
	e.g. separation of hydrogen or hydrogen	2200/54	in the low pressure column of a double pressure main column system
	containing gases form gaseous mixtures at low	2200/70	Refluxing the column with a condensed part of the
3/066	temperatures <u>C01B 3/506</u>)} • • • {separation of nitrogen (from air <u>F25J 3/04</u> ,	2200/70	feed stream, i.e. fractionator top is stripped or self-
3/000	production of nitrogen in general <u>C01B 21/00</u>)		rectified
3/0665	• • • {separation of carbon monoxide (production	2200/72	. Refluxing the column with at least a part of the
	of carbon monoxide containing gas in general		totally condensed overhead gas
	<u>C01B 32/40, C10J, C10K</u>)}	2200/74	Refluxing the column with at least a part of the
3/067	• • • {separation of carbon dioxide (production of	2200/74	partially condensed overhead gas
2/2/5	carbon dioxide in general <u>C01B 32/00</u>)}	2200/76	Refluxing the column with condensed overhead gas being cycled in a quasi-closed loop refrigeration
3/0675	• • • { separation of H ₂ /CO mixtures, i.e. of synthesis		cycle
	gas (production of carbon monoxide containing gas in general <u>C01B 32/40</u> , <u>C10J</u> , <u>C10K</u> ,	2200/78	Refluxing the column with a liquid stream
	production of hydrogen containing gas		originating from an upstream or downstream
	C01B 3/00)}		fractionator column

2210/14 • Coke-ovens gas

2200/80	· using integrated mass and heat exchange, i.e. non-	2210/18	• H ₂ /CO mixtures, i.e. synthesis gas; Water gas,
	adiabatic rectification in a reflux exchanger or dephlegmator		shifted synthesis gas or purge gas from HYCO synthesis
2200/90	• Details relating to column internals, e.g. structured	2210/20	• H ₂ /N ₂ mixture, i.e. synthesis gas for or purge gas
	packing, gas or liquid distribution		from ammonia synthesis
2200/92	Details relating to the feed point	2210/40	Air or oxygen enriched air, i.e. generally less than
2200/94	• Details relating to the withdrawal point		30mol% of O ₂
2200/96	Dividing wall column	2210/42	. Nitrogen
		2210/50	. Oxygen
<no title=""></no>	<u> </u>	2210/58	. Argon
2205/00	Processes or apparatus using other separation and/	2210/60	Natural gas or synthetic natural gas [SNG]
	or other processing means	2210/62	Liquefied natural gas [LNG]; Natural gas liquids
2205/02	• using simple phase separation in a vessel or drum		[NGL]; Liquefied petroleum gas [LPG]
2205/04	in the feed line, i.e. upstream of the fractionation	2210/66	• Landfill or fermentation off-gas, e.g. "Bio-gas"
	step	2210/70	Flue or combustion exhaust gas
2205/10	· using combined expansion and separation, e.g. in	2210/80	Carbon dioxide
	a vortex tube, "Ranque tube" or a "cyclonic fluid	2210/90	Boil-off gas from storage
	separator", i.e. combination of an isentropic nozzle	2215/00	Processes characterised by the type or other details
	and a cyclonic separator; Centrifugal separation		of the product stream
2205/20	 using solidification of components 	2215/02	Mixing or blending of fluids to yield a certain
2205/24	• using regenerators, cold accumulators or reversible		product
	heat exchangers	2215/04	Recovery of liquid products
2205/30	• using a washing, e.g. "scrubbing" or bubble column	2215/10	. Hydrogen
	for purification purposes	2215/14	Carbon monoxide
2205/32	as direct contact cooling tower to produce a	2215/18	• HYCO synthesis gas, e.g. H ₂ /CO mixture
	cooled gas stream, e.g. direct contact after cooler	2215/20	• Ammonia synthesis gas, e.g. H ₂ /N ₂ mixture
2205/24	[DCAC]	2215/30	. Helium
2205/34	 as evaporative cooling tower to produce chilled water, e.g. evaporative water chiller [EWC] 	2215/32	. Neon
2205/40	• using hybrid system, i.e. combining cryogenic and	2215/34	• Krypton
2203/40	non-cryogenic separation techniques	2215/36	. Xenon
2205/50	 using absorption, i.e. with selective solvents or 	2215/40	Air or oxygen enriched air, i.e. generally less than
2203/30	lean oil, heavier CnHm and including generally a		30mol% of O ₂
	regeneration step for the solvent or lean oil	2215/42	• Nitrogen or special cases, e.g. multiple or low purity
2205/60	• using adsorption on solid adsorbents, e.g. by		N_2
	temperature-swing adsorption [TSA] at the hot or	2215/44	• Ultra high purity nitrogen, i.e. generally less than
	cold end		1 ppb impurities
2205/62	Purifying more than one feed stream in multiple	2215/50	Oxygen or special cases, e.g. isotope-mixtures or
	1 1		
	adsorption vessels, e.g. for two feed streams at		low purity O_2
	different pressures	2215/52	$lacksquare$. Oxygen production with multiple purity O_2
2205/64	different pressures by pressure-swing adsorption [PSA] at the hot	2215/52 2215/54	* *
	different pressures • by pressure-swing adsorption [PSA] at the hot end		 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than
2205/64 2205/66	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of	2215/54 2215/56	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂
2205/66	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas	2215/54 2215/56 2215/58	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon
2205/66 2205/68	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas • Cooling the adsorption vessel	2215/54 2215/56 2215/58 2215/60	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane
2205/66 2205/68 2205/70	 different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Heating the adsorption vessel 	2215/54 2215/56 2215/58 2215/60 2215/62	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene
2205/66 2205/68	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas • Cooling the adsorption vessel • Heating the adsorption vessel • Pressurising or depressurising the adsorption	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene
2205/66 2205/68 2205/70 2205/72	 different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Heating the adsorption vessel Pressurising or depressurising the adsorption vessel 	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes
2205/66 2205/68 2205/70 2205/72 2205/80	 different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Heating the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step 	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82	 different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Heating the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step using a reactor with combustion or catalytic reaction 	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas • Cooling the adsorption vessel • Heating the adsorption vessel • Pressurising or depressurising the adsorption vessel • using membrane, i.e. including a permeation step • using a reactor with combustion or catalytic reaction • using filter	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas • Cooling the adsorption vessel • Heating the adsorption vessel • Pressurising or depressurising the adsorption vessel • using membrane, i.e. including a permeation step • using a reactor with combustion or catalytic reaction • using filter • using electrical phenomena, e.g. Corona discharge,	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas • Cooling the adsorption vessel • Heating the adsorption vessel • Pressurising or depressurising the adsorption vessel • using membrane, i.e. including a permeation step • using a reactor with combustion or catalytic reaction • using filter • using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas • Cooling the adsorption vessel • Heating the adsorption vessel • Pressurising or depressurising the adsorption vessel • using membrane, i.e. including a permeation step • using a reactor with combustion or catalytic reaction • using filter • using electrical phenomena, e.g. Corona discharge,	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86	different pressures • by pressure-swing adsorption [PSA] at the hot end • Regenerating the adsorption vessel, e.g. kind of reactivation gas • Cooling the adsorption vessel • Heating the adsorption vessel • Pressurising or depressurising the adsorption vessel • using membrane, i.e. including a permeation step • using a reactor with combustion or catalytic reaction • using filter • using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed stream
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86 2205/90	different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Heating the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step using a reactor with combustion or catalytic reaction using filter using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field Mixing of components	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed stream Separating impurities in general from the product
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86 2205/90	different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Heating the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step using a reactor with combustion or catalytic reaction using filter using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field Mixing of components Processes characterised by the type or other details	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00 2220/02	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed stream Separating impurities in general from the product stream
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86 2205/90 2210/00	different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Heating the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step using a reactor with combustion or catalytic reaction using filter using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field Mixing of components Processes characterised by the type or other details of the feed stream Multiple feed streams, e.g. originating from different sources	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00 2220/02	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed stream Separating impurities in general from the product stream Separating high boiling, i.e. less volatile components from air, e.g. CO₂, hydrocarbons Separating low boiling, i.e. more volatile
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86 2205/90 2210/00	different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step using a reactor with combustion or catalytic reaction using filter using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field Mixing of components Processes characterised by the type or other details of the feed stream Multiple feed streams, e.g. originating from different sources Mixing or blending of fluids with the feed stream	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00 2220/02 2220/04	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed stream Separating impurities in general from the product stream Separating high boiling, i.e. less volatile components from air, e.g. CO₂, hydrocarbons Separating low boiling, i.e. more volatile components from nitrogen, e.g. He, H₂, Ne
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86 2205/90 2210/00	different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step using a reactor with combustion or catalytic reaction using filter using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field Mixing of components Processes characterised by the type or other details of the feed stream Multiple feed streams, e.g. originating from different sources Mixing or blending of fluids with the feed stream Splitting of the feed stream, e.g. for treating or	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00 2220/02 2220/04	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed stream Separating high boiling, i.e. less volatile components from air, e.g. CO₂, hydrocarbons Separating low boiling, i.e. more volatile components from nitrogen, e.g. He, H₂, Ne Separating high boiling, i.e. less volatile
2205/66 2205/68 2205/70 2205/72 2205/80 2205/82 2205/84 2205/86 2205/90 2210/00 2210/02	different pressures by pressure-swing adsorption [PSA] at the hot end Regenerating the adsorption vessel, e.g. kind of reactivation gas Cooling the adsorption vessel Pressurising or depressurising the adsorption vessel using membrane, i.e. including a permeation step using a reactor with combustion or catalytic reaction using filter using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field Mixing of components Processes characterised by the type or other details of the feed stream Multiple feed streams, e.g. originating from different sources Mixing or blending of fluids with the feed stream	2215/54 2215/56 2215/58 2215/60 2215/62 2215/64 2215/66 2215/80 2220/00 2220/02 2220/04 2220/40	 Oxygen production with multiple purity O₂ Oxygen production with multiple pressure O₂ Ultra high purity oxygen, i.e. generally more than 99,9% O₂ Argon Methane Ethane or ethylene Propane or propylene Butane or mixed butanes Carbon dioxide Processes or apparatus involving steps for the removal of impurities Separating impurities in general from the feed stream Separating impurities in general from the product stream Separating high boiling, i.e. less volatile components from air, e.g. CO₂, hydrocarbons Separating low boiling, i.e. more volatile components from nitrogen, e.g. He, H₂, Ne

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2220/50	Separating low boiling, i.e. more volatile	2235/80	the fluid being carbon dioxide
	components from oxygen, e.g. N ₂ , Ar	2240/00	Processes or apparatus involving steps for
2220/52	Separating high boiling, i.e. less volatile	2240/00	expanding of process streams
	components from oxygen, e.g. Kr, Xe,	2240/02	Expansion of a process fluid in a work-extracting
2220/60	Hydrocarbons, Nitrous oxides, O ₃ • Separating impurities from natural gas, e.g.		turbine (i.e. isentropic expansion), e.g. of the feed
2220/00	mercury, cyclic hydrocarbons		stream
2220/62	• Separating low boiling components, e.g. He, H ₂ ,	2240/04	. Multiple expansion turbines in parallel
2220/02	N ₂ , Air	2240/10	• • the fluid being air
2220/64	Separating heavy hydrocarbons, e.g. NGL, LPG,	2240/12	• • the fluid being nitrogen
	C4+ hydrocarbons or heavy condensates in	2240/20	• • the fluid being oxygen
	general	2240/22	• the fluid being oxygen enriched compared to air,
2220/66	• • Separating acid gases, e.g. CO ₂ , SO ₂ , H ₂ S or RSH		e.g. "crude oxygen"
2220/68	Separating water or hydrates	2240/28	• the fluid being argon or crude argon
2220/80	• Separating impurities from carbon dioxide, e.g. H ₂ O	2240/30	Dynamic liquid or hydraulic expansion with
	or water-soluble contaminants		extraction of work, e.g. single phase or two-phase
2220/82	Separating low boiling, i.e. more volatile	2210110	turbine
	components, e.g. He, H ₂ , CO, Air gases, CH ₄	2240/40	Expansion without extracting work, i.e. isenthalpic
2220/84	Separating high boiling, i.e. less volatile		throttling, e.g. JT valve, regulating valve or venturi,
	components, e.g. NOx, SOx, H2S	2240/42	or isentropic nozzle, e.g. Laval
2220/90	• Separating isotopes of a component, e.g. H ₂ , O ₂	2240/42	. the fluid being air
2230/00	Processes or apparatus involving steps for	2240/44	the fluid being nitrogen the fluid being oxygen
2230/00	increasing the pressure of gaseous process streams	2240/48	 the fluid being oxygen enriched compared to air,
2230/02	Compressor intake arrangement, e.g. filtering or	2240/46	e.g. "crude oxygen"
2200/02	cooling	2240/60	Expansion by ejector or injector, e.g.
2230/04	Compressor cooling arrangement, e.g. inter- or	2240/00	"Gasstrahlpumpe", "venturi mixing", "jet pumps"
	after-stage cooling or condensate removal	2240/70	Steam turbine, e.g. used in a Rankine cycle
2230/06	Adiabatic compressor, i.e. without interstage	2240/80	Hot exhaust gas turbine combustion engine
	cooling	2240/82	with waste heat recovery, e.g. in a combined
2230/08	• Cold compressor, i.e. suction of the gas at cryogenic	2240/02	cycle, i.e. for generating steam used in a Rankine
	temperature and generally without afterstage-cooler		cycle
2230/20	 Integrated compressor and process expander; 	2240/90	Hot gas waste turbine of an indirect heated gas for
	Gear box arrangement; Multiple compressors on a common shaft		power generation
2230/22	Compressor driver arrangement, e.g. power supply	2245/00	Processes or apparatus involving steps for
	by motor, gas or steam turbine		recycling of process streams
2230/24	 Multiple compressors or compressor stages in 	2245/02	Recycle of a stream in general, e.g. a by-pass stream
	parallel	2245/40	
2220/20			the recycled stream being air
2230/30	. Compression of the feed stream	2245/42	the recycled stream being nitrogen
2230/32	Compression of the product stream	2245/42 2245/50	 the recycled stream being nitrogen the recycled stream being oxygen
2230/32 2230/40	Compression of the product stream the fluid being air	2245/42 2245/50 2245/58	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon
2230/32 2230/40 2230/42	Compression of the product streamthe fluid being airthe fluid being nitrogen	2245/42 2245/50	 the recycled stream being nitrogen the recycled stream being oxygen
2230/32 2230/40 2230/42 2230/50	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen 	2245/42 2245/50 2245/58 2245/90	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage
2230/32 2230/40 2230/42	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, 	2245/42 2245/50 2245/58 2245/90 2250/00	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers
2230/32 2230/40 2230/42 2230/50 2230/52	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" 	2245/42 2245/50 2245/58 2245/90	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon 	2245/42 2245/50 2245/58 2245/90 2250/00	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers
2230/32 2230/40 2230/42 2230/50 2230/52	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of 	2245/42 2245/50 2245/58 2245/90 2250/00	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2230/80	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/10	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2230/80	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/10	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2230/80	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/10	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general,
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2230/80 2235/00	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/10 2250/20	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2230/80 2235/00	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/20	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2235/00 2235/00	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator Lifting of liquids by gas lift, e.g. "Mammutpumpe" 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/30	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid One fluid being air
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2235/00 2235/00	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/30 2250/40 2250/42	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid One fluid being air One fluid being nitrogen
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2235/00 2235/02 2235/04 2235/06 2235/42 2235/50	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator Lifting of liquids by gas lift, e.g. "Mammutpumpe" the fluid being nitrogen the fluid being oxygen 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/30 2250/40 2250/40 2250/42 2250/50	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid One fluid being air One fluid being nitrogen One fluid being oxygen
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2235/00 2235/02 2235/04 2235/06 2235/06 2235/42	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator Lifting of liquids by gas lift, e.g. "Mammutpumpe" the fluid being oxygen the fluid being oxygen enriched compared to air 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/30 2250/40 2250/42	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid One fluid being air One fluid being nitrogen One fluid being oxygen One fluid being oxygen enriched compared to air,
2230/32 2230/40 2230/40 2230/50 2230/52 2230/58 2230/60 2235/00 2235/00 2235/04 2235/06 2235/06 2235/22 2235/50 2235/50	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator Lifting of liquids by gas lift, e.g. "Mammutpumpe" the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air ("crude oxygen") 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/30 2250/40 2250/40 2250/42 2250/50 2250/52	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid One fluid being air One fluid being nitrogen One fluid being oxygen One fluid being oxygen enriched compared to air, e.g. "crude oxygen"
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2235/00 2235/00 2235/04 2235/06 2235/42 2235/50 2235/52	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator Lifting of liquids by gas lift, e.g. "Mammutpumpe" the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air ("crude oxygen") the fluid being argon or crude argon 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/30 2250/40 2250/40 2250/42 2250/50	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid One fluid being air One fluid being nitrogen One fluid being oxygen One fluid being oxygen enriched compared to air,
2230/32 2230/40 2230/42 2230/50 2230/52 2230/58 2230/60 2235/00 2235/02 2235/04 2235/06 2235/06 2235/42 2235/50 2235/52	 Compression of the product stream the fluid being air the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air, e.g. "crude oxygen" the fluid being argon or crude argon the fluid being hydrocarbons or a mixture of hydrocarbons the fluid being carbon dioxide Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams using a pump in general or hydrostatic pressure increase using a pressure accumulator Lifting of liquids by gas lift, e.g. "Mammutpumpe" the fluid being nitrogen the fluid being oxygen the fluid being oxygen enriched compared to air ("crude oxygen") 	2245/42 2245/50 2245/58 2245/90 2250/00 2250/02 2250/04 2250/20 2250/30 2250/40 2250/40 2250/42 2250/50 2250/52	 the recycled stream being nitrogen the recycled stream being oxygen the recycled stream being argon or crude argon the recycled stream being boil-off gas from storage Details related to the use of reboiler-condensers Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film Boiler-condenser with superposed stages Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid One fluid being air One fluid being nitrogen One fluid being oxygen One fluid being oxygen enriched compared to air, e.g. "crude oxygen"

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2260/00	Coupling of processes or apparatus to other units; Integrated schemes	2270/902	Details about the refrigeration cycle used, e.g. composition of refrigerant, arrangement of
2260/02	Integration in an installation for exchanging heat, e.g. for waste heat recovery		compressors or cascade, make up sources, use of reflux exchangers etc.
2260/10	Integration in a gas transmission system at a	2270/904	by liquid or gaseous cryogen in an open loop
	pressure reduction, e.g. "let down" station	2270/906	by heat driven absorption chillers
2260/20	Integration in an installation for liquefying or solidifying a fluid stream	2270/908	 by regenerative chillers, i.e. oscillating or dynamic systems, e.g. Stirling refrigerator,
2260/30	Integration in an installation using renewable energy		thermoelectric ("Peltier") or magnetic
2260/30	Integration in an installation using renewable energy Integration in an installation using nitrogen, e.g.		refrigeration
2200/42	as utility gas, for inerting or purging purposes	2270/91	using pulse tube refrigeration
	in IGCC, POX, GTL, PSA, float glass forming, incineration processes, for heat recovery or for enhanced oil recovery	2270/912	Liquefaction cycle of a low-boiling (feed) gas in a cryocooler, i.e. in a closed-loop refrigerator
2260/44	using nitrogen for cooling purposes	2280/00	Control of the process or apparatus
2260/50	Integration in an installation using oxygen, e.g. in	2280/02	Control in general, load changes, different modes
2200/30	the burner of a glass facility, waste incineration or		("runs"), measurements
	oxygen based process [OBP] in general	2280/10	• Control for or during start-up and cooling down of
2260/58	Integration in an installation using argon	2200/20	the installation
2260/60	Integration in an installation using hydrocarbons,	2280/20	• Control for stopping, deriming or defrosting after an
	e.g. for fuel purposes		emergency shut-down of the installation or for back
2260/80	. Integration in an installation using carbon dioxide,	2280/30	up system Control of a discontinuous or intermittent ("batch")
	e.g. for EOR, sequestration, refrigeration etc.	2280/30	Control of a discontinuous or intermittent ("batch") process
2270/00	Refrigeration techniques used	2280/40	Control of freezing of components
2270/02	Internal refrigeration with liquid vaporising loop	2280/50	Advanced process control, e.g. adaptive or
2270/02	Internal refrigeration with mquid vaporising loop Internal refrigeration with work-producing gas	2200/30	multivariable control
2210/04	expansion loop		
2270/06	with multiple gas expansion loops	2290/00	Other details not covered by groups
2270/08	Internal refrigeration by flash gas recovery loop	2200/02	<u>F25J 2200/00</u> - <u>F25J 2280/00</u>
2270/12	External refrigeration with liquid vaporising loop	2290/02	Comparison of processes or apparatuses
2270/14	External refrigeration with work-producing gas	2290/10	Mathematical formulae, modeling, plot or curves; Design methods.
	expansion loop	2290/12	Design methods • Particular process parameters like pressure,
2270/16	• with mutliple gas expansion loops of the same refrigerant		temperature, ratios
2270/18	External refrigeration with incorporated cascade	2290/20 2290/30	Particular dimensions; Small scale or microdevices Details about heat insulation or cold insulation
	loop	2290/30	
2270/20	Quasi-closed internal or closed external hydrogen	2290/32	 Details on header or distribution passages of heat exchangers, e.g. of reboiler-condenser or plate heat
	refrigeration cycle		exchangers exchangers
2270/24	Quasi-closed internal or closed external carbon	2290/34	Details about subcooling of liquids
	monoxide refrigeration cycle	2290/40	Vertical layout or arrangement of cold equipments
2270/30	Quasi-closed internal or closed external helium refrigeration cycle	, , , , ,	within in the cold box, e.g. columns, condensers,
2270/40	Quasi-closed internal or closed external air		heat exchangers etc.
2270/10	refrigeration cycle	2290/42	Modularity, pre-fabrication of modules, assembling
2270/42	• Quasi-closed internal or closed external nitrogen		and erection, horizontal layout, i.e. plot plan, and vertical arrangement of parts of the cryogenic unit,
	refrigeration cycle		e.g. of the cold box
2270/50	Quasi-closed internal or closed external oxygen	2290/44	• Particular materials used, e.g. copper, steel or alloys
2270/58	refrigeration cycle • Quasi-closed internal or closed external argon	2250,	thereof or surface treatments used, e.g. enhanced surface
	refrigeration cycle	2290/50	Arrangement of multiple equipments fulfilling the
2270/60	Closed external refrigeration cycle with single	2270/20	same process step in parallel
	component refrigerant [SCR], e.g. C1-, C2- or C3-hydrocarbons	2290/60	Details about pipelines, i.e. network, for feed or product distribution
2270/66	Closed external refrigeration cycle with multi	2290/62	Details of storing a fluid in a tank
	component refrigerant [MCR], e.g. mixture of	2290/70	 Processing device is mobile or transportable, e.g. by
	hydrocarbons		hand, car, ship, rocket engine etc.
2270/80	Quasi-closed internal or closed external carbon dioxide refrigeration cycle	2290/72	• Processing device is used off-shore, e.g. on a
2270/88	Quasi-closed internal refrigeration or heat pump		platform or floating on a ship or barge
2210/00	cycle, if not otherwise provided	2290/80	Retrofitting, revamping or debottlenecking of
2270/90	External refrigeration, e.g. conventional closed-loop		existing plant
2210170	mechanical refrigeration unit using Freon or NH ₃ ,	2290/90	Details about safety operation of the installation